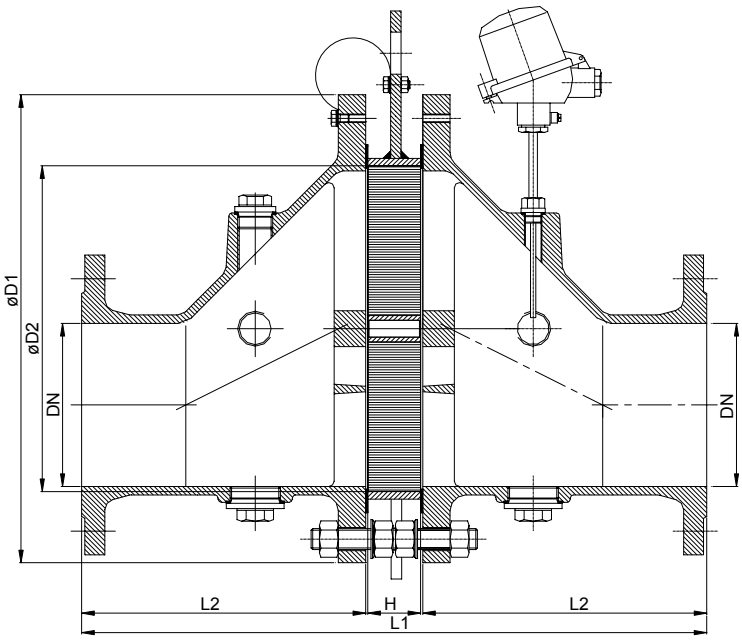
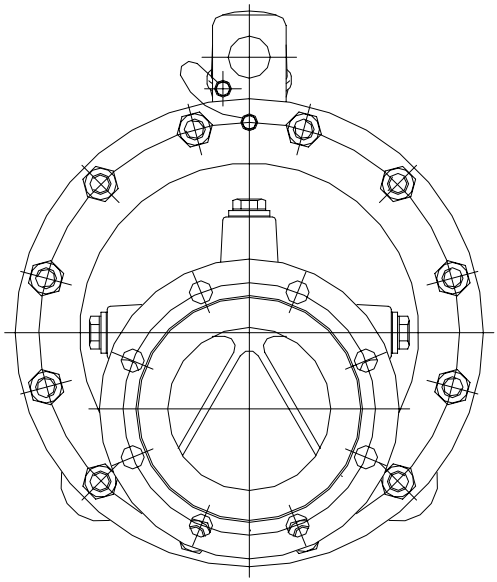
Bi-directional deflagration flame arrester
KITO EFA-Def-I-…/…
KITO EFA-Def-I-…/…T





size	DN	ANSI	D1	D2	L1	H	L2	kg
65	**25**	**1“**	155	70	264	20	120	
	32	**1 ¼“**						
100	**40**	**1 ½“**	220	106	314	20	145	22
	50	**2“**						23
150	**50**	**2“**	285	159	374	20	175	33
	65	**2 ½“**						35
	80	**3“**						40
200	**80**	**3“**	340	206	424	20	200	50
	100	**4“**						54
300	**100**	**4“**	445	308	564	20	270	
	125	**5“**						94
	150	**6“**						100
400	**150**	**6“**	565	388	654	20	315	
	200	**8“**						
500	**200**	**8“**	670	485	784	20	380	230
	250	**10“**						
600	**250**	**10“**	780	584	924	20	450	
	300	**12“**						

Type examination certificate in accordance to ATEX 100 a and EN 12874

CE - marking available

Example for orders :
KITO EFA-Def-I-300/150T
(flame arrester including temperature sensor)

Dimensions in mm

Design subject to change

Performance curves : H 0.27 N

Standard design

housing	: cast steel 1.0619, 1.4408
gasket	: HD 3822, PTFE
casing for grid	: 1.0305, 1.4571, 1.4581
grid	: 1.4310, 1.4571, strip thickness 0.15 mm
bolts/nuts	: galvanized steel, SS
temperature sensor	: PT 100 (option)
flange connection	: DIN 2501 PN 10 ANSI 150 lbs. RF

Other materials, special designs, heating etc. upon request.

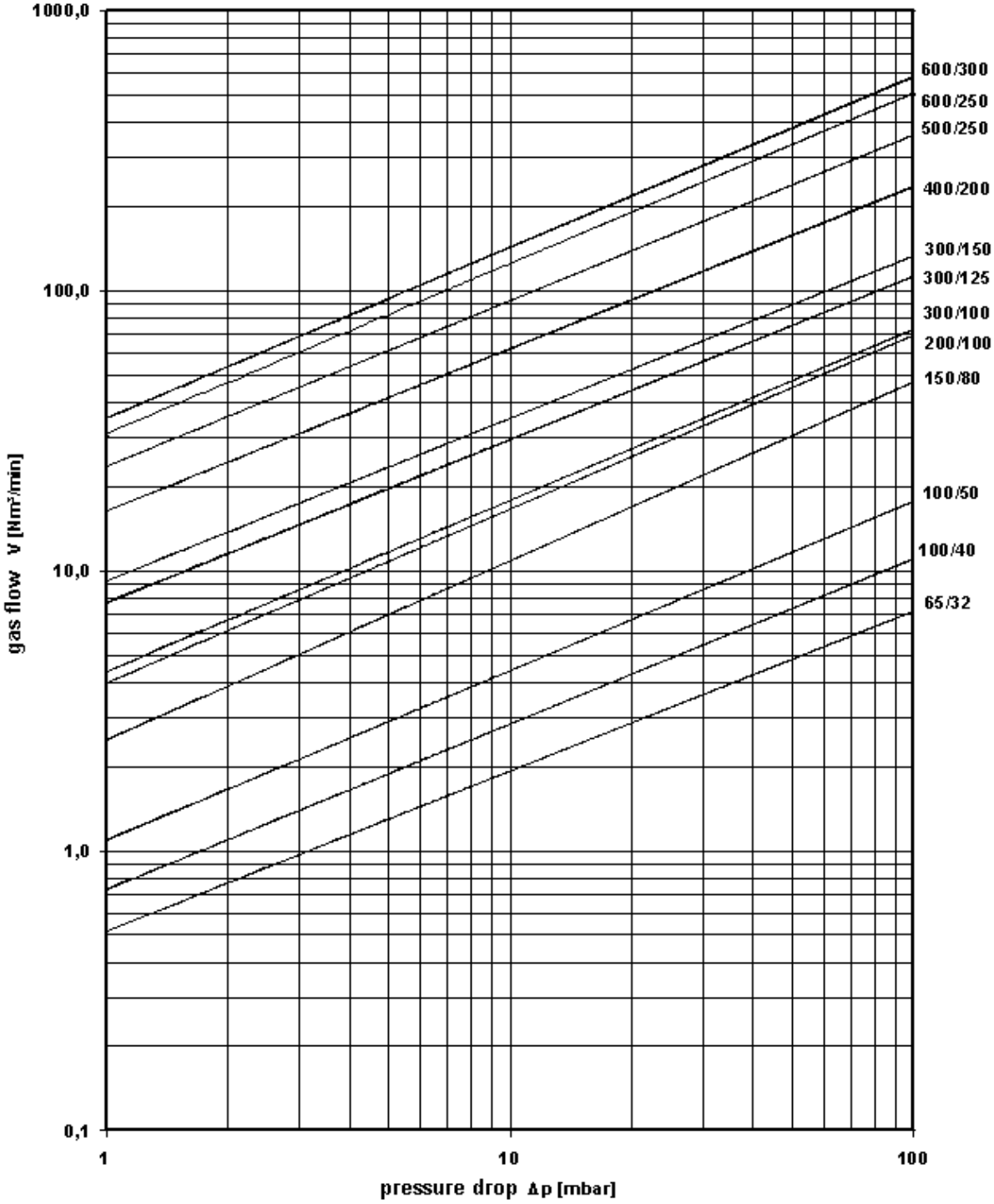
Application

For installation into pipelines to the protection of containers and components against deflagration of flammable liquids and gases.
Approved for all materials of the explosion group I with a maximum experimental safe gap (MESG) ≥ 1.1 mm.
Preventing flame transmission from both sides in pipelines operating under atmospheric conditions (operating pressure ≤ 1.1 bar abs).
Provided with one or two temperature sensors (PT 100) the flame arrester is safe against short time burning from one or both sides.
If only one thermal sensor is attached, it must be installed into that part of the body from which a fire is expected.
The distance between the possible ignition source and the flame arrester must not exceed 50 times the inner pipe diameter.
The installation of the deflagration flame arrester into horizontal and vertical pipelines is permissible.

The flow capacity V refers to a density of air with ρ = 1.29 kg/m³ at T = 273 K and a pressure of p = 1.013 mbar

The flow capacity for gases with different densities can be calculated sufficiently accurate by the following approximation equation:

$$\dot{V} = \dot{V}_b \cdot \sqrt{\frac{\rho_b}{1{,}29}} \qquad or \qquad \dot{V}_b = \dot{V} \cdot \sqrt{\frac{1{,}29}{\rho_b}}$$



Design subject to change