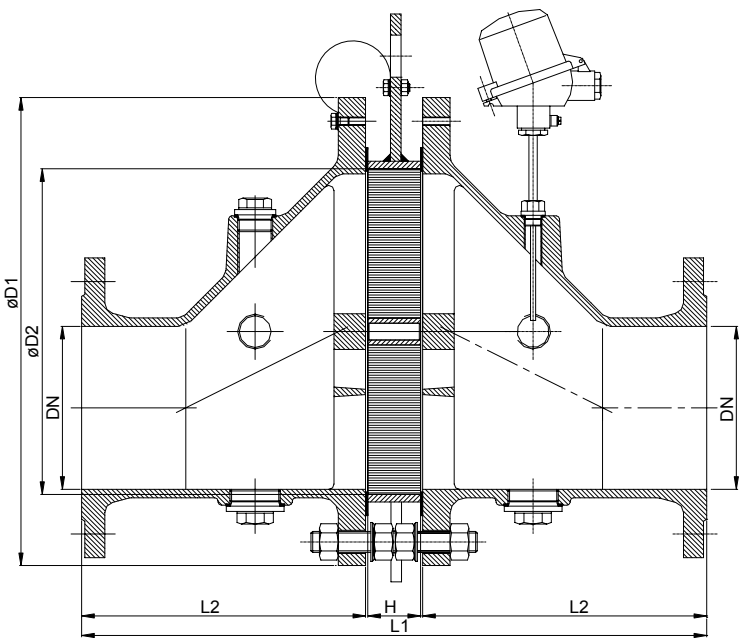
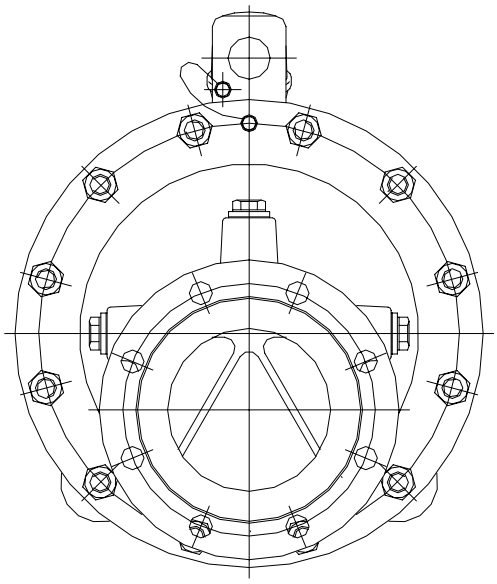
Bi-directional in-line detonation flame arrester
KITO EFA-Det-IIB3-…/…
KITO EFA-Det-IIB3-…/…-T





size	DN	ANSI	D1	D2	L1	H	L2	kg
65	**25**	**1“**	155	70	308	64	120	
	32	**1 ¼“**						
100	**40**	**1 ½“**	220	106	358	64	145	
	50	**2“**						
150	**50**	**2“**	285	159	418	64	175	42
	65	**2 ½“**						
	80	**3“**						
200	**80**	**3“**	340	206	468	64	200	
	100	**4“**						
300	**100**	**4“**	445	308	630	86	270	
	125	**5“**						
	150	**6“**						
400	**150**	**6“**	565	388	720	86	315	
	200	**8“**						
500	**200**	**8“**	670	485	850	86	380	
	250	**10“**						
600	**250**	**10“**	780	584	990	86	450	
	300	**12“**						

EC type approval
ATEX 100 a and EN 12874

CE -designation
available

Example to order :
KITO EFA-Det-IIB3-300/150-T
(design with temperature sensor)

dimension in mm

Design subject to change

For performance curves see diagram : G 0.18 N

Standard design

housing	: cast steel 1.0619, 1.4408
gasket	: HD 3822, PTFE
casing for grid	: 1.0305, 1.4571, 1.4571
grid	: 1.4310, 1.4571, strip thickness 0.15 mm
bolts/nuts	: galvanized steel, SS
temperature sensor	: PT 100 (option)
flange connection	: DIN 2501 PN 10 ANSI 150 lbs

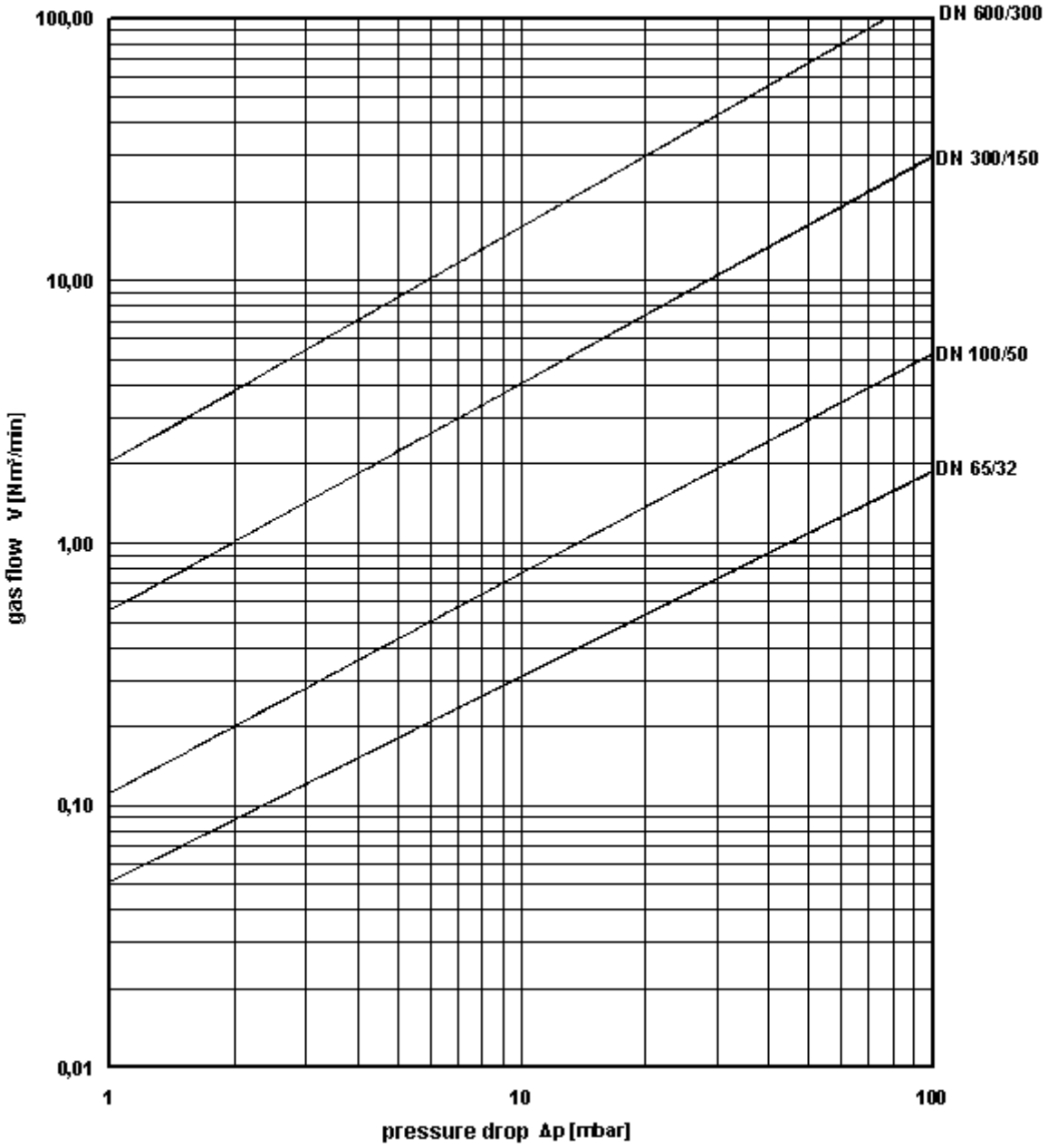
Other materials, special designs, heating etc. upon request.

Application

For installation into pipelines to the protection of containers and components against **stable** detonation of flammable liquids and gases.
Approved for all materials of the explosion group IIB1,IIB2 and IIB3 with a maximum experimental safe gap (MESG) > 0.65 mm.
Preventing flame transmission from both sides in pipelines operating under atmospheric conditions (operating pressure ≤ 1.1 bar abs).
Provided with one or two temperature sensors (PT 100) the armature is safe against short time burning from one or both sides. If only one thermal sensor is attached, it must be installed into that part of the detonation flame arrester from which a fire is expected.
The installation of the detonation flame arrester into horizontal and vertical pipelines is permissible.

Flow capacity V based on air of a density ρ = 1.29 kg/m³ at T = 273 K and atmospheric pressure p = 1.013 mbar.

For other gases the flow can be approximately calculated by $\dot{V} = \dot{V}_b \cdot \sqrt{\frac{\rho_b}{1{,}29}}$ *or* $\dot{V}_b = \dot{V} \cdot \sqrt{\frac{1{,}29}{\rho_b}}$



Design subject to change